

# Distributed order PID optimization in comparison with fractional PID optimization based on performance and robustness indices

Boris B. Jakovljević, Tomislav B. Šekara, Milan R. Rapaić, Zoran D. Jeličić

**Abstract**—This paper presents a comparison of most frequently used criteria for optimizing distributed order PID and fractional PID controllers. The problem of interest is how to provide load disturbance rejection under constraints to performance and robustness. The comparison of optimal controllers via different optimization criteria has been performed for different non-integer processes. The optimal controllers are obtained via optimization by genetic algorithm.

## I. INTRODUCTION

PID controllers have been very popular among engineers and scientist, [1], [2]. Their popularity became significant due to their simplicity, small number of parameters to be tuned and the fact that it is not necessary to know the exact model of process in order to properly tune the controller. The development in the field of fractional calculus introduced a new PID-like structures that have proved themselves in different aspects [3], [4], [5]. These PID modifications introduce complexity in the controller's structure, but in the same way improve robustness in comparison with performance or vice versa. In order to tune an optimal controller some aspects must be taken into account. System in demand must conform itself to the constraints on robustness and performance as well to stay stable. These aspects of performance and robustness can be various and in this paper only the most commonly used will be presented.

The most usual problems for which the controllers are tuned are the reference tracking or disturbance rejection. The frequently considered system is given in Fig. 1. This paper treats the problem of finding an optimal controller for unit step disturbance rejection. The optimal controllers for different demands on robustness and performance are found and compared in the sense of response quality.

The paper is organized as follows: Section II gives an overview of PID-like structures, Section III presents the most commonly used performance and robustness indices, while Section IV presents the optimization problems and Section V shows the optimization results. Last section concludes the paper.

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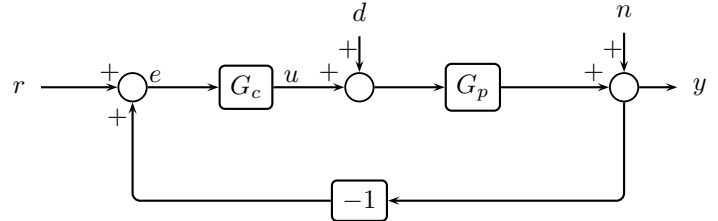


Fig. 1. Plant  $G_p(s)$  with dPID controller  $G_c(s)$ . Reference signal is denoted by  $r$  (assumably  $r=0$ ), load disturbance by  $d$ , measurement noise by  $n$ , control signal by  $u$ , error signal by  $e$  and system output by  $y$ .

## II. PID-LIKE STRUCTURES

Classical PID controller can be described by different structures but the most usual is parallel controller which is defined by the following differential equation as

$$u_{pid}(t) = k_p e(t) + k_i \int_0^t e(\tau) d\tau + k_d \frac{de(t)}{dt}, \quad (1)$$

where  $k_p$ ,  $k_i$ ,  $k_d$  represent proportional gain, integral gain, derivative gain, respectively.  $e(t)$  represents error signal, while  $u_{pid}(t)$  represents control signal.

The transfer function of the classical PID with noise cancellation filter is given by

$$G_{pid}(s) = \frac{k_p + k_i \frac{1}{s} + k_d s}{T_f s + 1} \quad (2)$$

where  $T_f$  represents filter's time constant.

Compared to a classical PID controller, FPID has two additional degrees of freedom – the integration order  $\alpha$  and the differentiation order  $\beta$ . These two newly introduced degrees of freedom provide more flexibility in applications but in the same time complicate the controller's structure.

$$G_{fpid}(s) = \frac{k_p + k_i \frac{1}{s^\alpha} + k_d s^\beta}{(T_f s + 1)^\beta}. \quad (3)$$

By generalization of fractional PID controller, one can acquire a distributed order PID. The distributed order PID controller with noise cancellation filter is given by

$$G_{dopid}(s) = \frac{1}{T_f s + 1} \sum_{i=0}^{N-1} k_i s^{-1+i\Delta\alpha}. \quad (4)$$

with  $k_i$  being the gains of differintegrators and  $odd$  integer  $N > 1$  being the number of differintegrators and a positive step length calculated as  $\Delta\alpha = \frac{2}{N-1}$

The more details about the DOPID structure can be found in [3], [6].

### III. PERFORMANCE AND ROBUSTNESS INDICES

Integral of absolute error (IAE) is perhaps the most frequently used as performance measure, defined as

$$IAE = \int_0^{\infty} |e(t)| dt. \quad (5)$$

One more frequently used performance indexes when considering PID controllers is Integral of error (IE) and it is defined as

$$IE = \int_0^{\infty} e(t) dt. \quad (6)$$

There exists a direct dependence between integral gain,  $k_i$ , and integral of error (IE) in the case when load disturbance is constant unit signal [1].

Very often used performance index regarding noise influence is maximal sensitivity to measurement noise  $M_n$

$$M_n = \max_{\omega \geq 0} \left| \frac{-G_c(j\omega)}{1 + G_c(j\omega)G_p(j\omega)} \right| \quad (7)$$

as it equals  $\frac{k_d}{T_f}$  for classical PID controllers and DOPID controllers and  $\frac{k_d}{T_f^\beta}$  for FPID controllers.

If one wants to guarantee robustness to model uncertainties, maximum sensitivity  $M_s$  was considered to be less than a specified value.  $M_s$  is given with

$$M_s = \max_{\omega \geq 0} \left| \frac{1}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_s}. \quad (8)$$

The index that constraints the maximum resonant peak is defined as

$$Q = \max_{\omega \geq 0} \left| \frac{k_i \frac{G_p(j\omega)}{j\omega}}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_q}. \quad (9)$$

Šekara and Mataušek showed in [8] that constraining  $Q$  to be less than 1.01 provides acceptable values of IAE.

One more frequently used robustness index, often in combination with  $M_s$  is Maximum complementary sensitivity defined as

$$M_p = \max_{\omega \geq 0} \left| \frac{G_c(j\omega)G_p(j\omega)}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_p}. \quad (10)$$

Perhaps, one not so conventional performance index is the maximization of minimum of amplitude characteristic of controller, of course over complete frequency range, as it reduces the influence of load disturbance. This can be described as

$$M_{min}A = \max_{\omega \geq 0} (\min |G_c(j\omega)|). \quad (11)$$

The last index coincides with maximization of proportional gain  $k_p$  at classical PID controllers [7].

### IV. OPTIMIZATION PROBLEMS

For all optimization problems in this research the issue was to find an optimal controller FPID and DOPID in order to reject load disturbance and closed loop system is stable. The optimization in all cases was performed by particle swarm optimization algorithm. The processes that were analyzed are the following non-integer processes

$$G_{p1}(s) = \frac{-(1-s)\ln(s)}{(s+1)^3}, \quad (12)$$

$$G_{p2}(s) = \frac{-(1-s)\ln(s)}{(s+1)^2}. \quad (13)$$

The following optimization problems were analyzed.

#### A. Optimization problem 1 (OP1)

This optimization problem is formulated for DOPID controller with  $N = 7$  differintegrators of the form

$$G_{\text{dopid},7}(s) = \frac{1}{sT_f + 1} \left( k_0 \frac{1}{s} + k_1 \frac{1}{s^{2/3}} + \dots + k_5 s^{2/3} + k_6 s \right). \quad (14)$$

The controller is optimized with the following concerns

$$\max_{k_0, k_1, \dots, k_6, \omega_q, \omega_s} k_3, \quad (15)$$

$$T_f = \frac{k_d}{M_n^{\max}}, \quad (16)$$

$$M_s = \left| \frac{1}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_s} \leq M_s^{\max}, \quad (17)$$

$$Q = \left| \frac{k_i \frac{G_p(j\omega)}{j\omega}}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_q} \leq Q^{\max}, \quad (18)$$

$$k_i \geq k_i^{\min}, i \in \{0, \dots, N-1\}. \quad (19)$$

The same was observed for FPID controller, so the only difference in this case is in the first equation, i.e. in the controller structure.

#### B. Optimization problem 2 (OP2)

This optimization problem is formulated for DOPID controller of the same structure as for optimization problem 1.

$$\max_{k_0, k_1, \dots, k_6, \omega_q, \omega_s} k_0, \quad (20)$$

The controller is optimized with the following concerns

$$T_f = \frac{k_d}{M_n^{\max}}, \quad (21)$$

$$M_s = \left| \frac{1}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_s} \leq M_s^{\max}, \quad (22)$$

$$Q = \left| \frac{k_i \frac{G_p(j\omega)}{j\omega}}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_q} \leq Q^{\max}, \quad (23)$$

$$k_i \geq k_i^{\min}, i \in \{0, \dots, N-1\}. \quad (24)$$

The same was observed for FPID controller, so the only difference in this case is in the first equation, i.e. in the controller structure.

### C. Optimization problem 3 (OP3)

This optimization problem is formulated for DOPID controller of the same structure as for optimization problem 1.

$$\max_{k_0, k_1, \dots, k_6, \omega_q, \omega_s} k_0, \quad (25)$$

The controller is optimized with the following concerns

$$T_f = \frac{k_d}{M_n^{\max}}, \quad (26)$$

$$M_s = \left| \frac{1}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_s} \leq M_s^{\max}, \quad (27)$$

$$M_p = \max_{\omega \geq 0} \left| \frac{G_c(j\omega)G_p(j\omega)}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_p} \leq M_p^{\max}, \quad (28)$$

$$k_i \geq k_i^{\min}, i \in \{0, \dots, N-1\}. \quad (29)$$

The same was observed for FPID controller, so the only difference in this case is in the first equation, i.e. in the controller structure.

### D. Optimization problem 4 (OP4)

This optimization problem is formulated for DOPID controller of the same structure as for optimization problem 1.

The controller is optimized with the following concerns

$$\max_{k_0, k_1, \dots, k_6, \omega_q, \omega_s} k_3, \quad (30)$$

$$T_f = \frac{k_d}{M_n^{\max}}, \quad (31)$$

$$M_s = \left| \frac{1}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_s} \leq M_s^{\max}, \quad (32)$$

$$Q = \left| \frac{k_i \frac{G_p(j\omega)}{j\omega}}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_q} \leq Q^{\max}, \quad (33)$$

$$M_p = \max_{\omega \geq 0} \left| \frac{G_c(j\omega)G_p(j\omega)}{1 + G_c(j\omega)G_p(j\omega)} \right|_{\omega=\omega_p} \leq M_p^{\max}, \quad (34)$$

$$k_i \geq k_i^{\min}, i \in \{0, \dots, N-1\}. \quad (35)$$

This optimization problem has one more constraint compared to all other optimization problems considered so far. For this problem it was impossible to find neither optimal FPID nor classical PID controller.

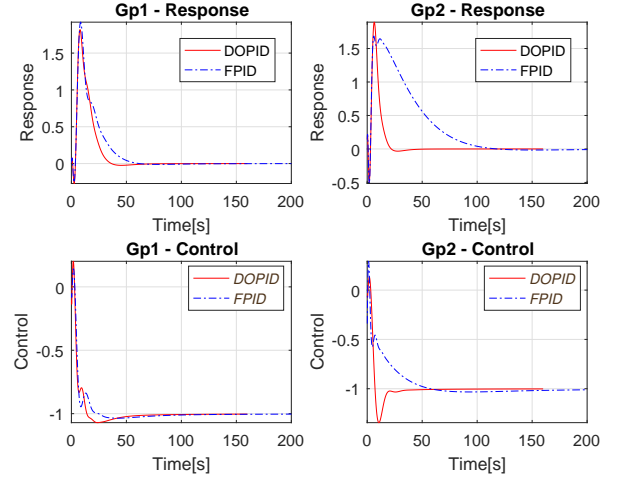


Fig. 2. Optimization problem 1: Response and control signal on unit step load disturbance  $d(t)$  for process  $G_{p1}$  on the left and response and control signal for process  $G_{p2}$  on the right controlled by FPID and DOPID under constraints  $M_s^{\max} = 2$ ,  $M_n^{\max} = 20$  and  $Q^{\max} = 1.01$ .

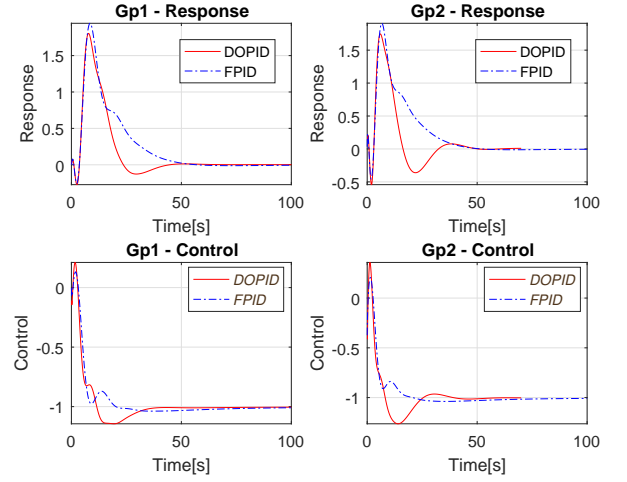


Fig. 3. Optimization problem 2: Response and control signal on unit step load disturbance  $d(t)$  for process  $G_{p1}$  on the left and response and control signal for process  $G_{p2}$  on the right controlled by FPID and DOPID under constraints  $M_s^{\max} = 2$ ,  $M_n^{\max} = 20$  and  $Q^{\max} = 1.01$ .

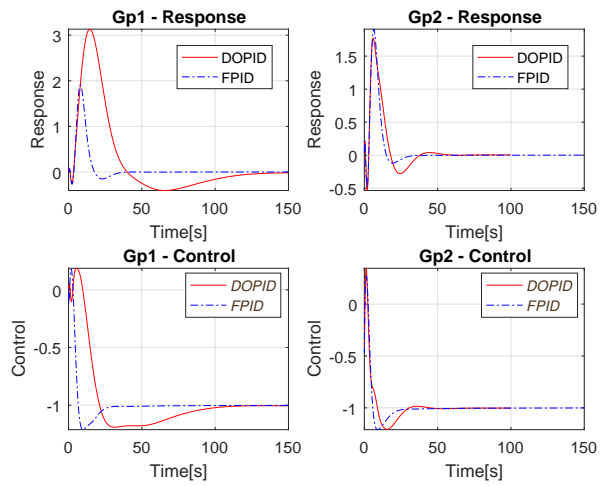


Fig. 4. Optimization problem 3: Response and control signal on unit step load disturbance  $d(t)$  for process  $G_{p1}$  on the left and response and control signal for process  $G_{p2}$  on the right controlled by FPID and DOPID under constraints  $M_s^{max} = 2$ ,  $M_n^{max} = 20$  and  $M_p^{max} = 1.3$ .

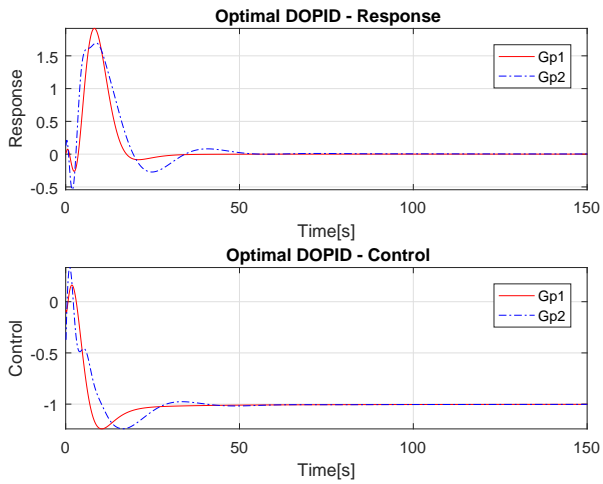


Fig. 5. Optimization problem 4: Responses on unit step load disturbance  $d(t)$  for processes  $G_{p1}$  and  $G_{p2}$  above and control signals for processes  $G_{p1}$  and  $G_{p2}$  on bottom, for optimal DOPID controller under constraints  $M_s^{max} = 2$ ,  $M_n^{max} = 20$  and  $M_p^{max} = 1.3$ .

TABLE I  
OPTIMAL PARAMETERS OF FPID AND DOPID CONTROLLER FOR PROCESSES  $G_{p1}, G_{p2}$  FOR CONSTRAINTS VALUES  $M_n^{max} = 20, M_s^{max} = 2,$   
 $M_p^{max} = 1.3$  AND  $Q^{max} = 1.01$  FOR OPTIMIZATION PROBLEMS 1, 2, 3; RESULTS FOR FPID CONTROLLER ARE MARKED WITH \*.

OP	Proc.	$k_0/k_i$	$k_1/\alpha$	$k_2/\beta$	$k_3/k_p$	$k_4$	$k_5$	$k_6/k_d$	$T_f$	IAE	$M_p / Q$
OP1	$G_{p1}$	4.96e-2	-2.15e-3	2.53e-2	0.317	-3.58e-2	4.81e-3	6.22e-1	3.11e-2	22.33	1.06
OP1	$G_{p1}^*$	3.68e-2	1	1	0.378	/	/	4.85e-1	1.89e-2	29.37	1.03
OP1	$G_{p2}$	8.19e-2	7.09e-3	4.14e-3	0.361	1.23e-2	7.35e-4	2.74e-1	1.37e-2	14.48	1.13
OP1	$G_{p2}^*$	1.66e-2	1	0.94	0.256	/	/	3.56e-2	1.34e-2	64.87	1.04
OP2	$G_{p1}$	6.14e-2	7.90e-3	4.23e-2	2.19e-1	2.15e-2	-5.74e-4	6.66e-01	3.33e-2	19.61	1.16
OP2	$G_{p1}^*$	4.05e-2	1	1	3.84e-1	/	/	2.8e-1	1.39e-2	26.78	1.06
OP2	$G_{p2}$	7.04e-2	2.65e-1	-7.65e-1	1.26	-5.11e-1	4.42e-4	5.00e-01	2.5e-2	18.32	1.42
OP2	$G_{p2}^*$	4.50e-2	1	1	3.79e1	/	/	1.71e-1	8.53e-3	24.70	1.03
OP3	$G_{p1}$	3.82e-2	-8.86e-2	5.91e-2	3.53e-1	-4.08e-1	-6.20e-1	4.65e-1	2.32e-2	78.12	<b>2.47</b>
OP3	$G_{p1}^*$	9e-2	1	1	3.86e-1	/	/	4.85e-1	2.42e-2	15.37	<b>1.16</b>
OP3	$G_{p2}$	7.27e-2	2.24e-1	-7.49e-1	1.32	-4.93e-1	-6.80e-2	5.13e-1	2.57e-2	18.42	<b>1.05</b>
OP3	$G_{p2}^*$	1.05e-1	1	1	3.76e-1	/	/	2.88e-1	1.44e-2	13.48	<b>1.13</b>

## V. RESULTS

Table I shows the optimal parameters of all controllers for all optimization problems considered in this paper as well as the values of indices of interest. Figs. 2, 3, 4 show the responses and control signals for all optimization problems for all considered processes. Fig. 5 shows the results of response and control signals for optimal DOPID controllers for both observed processes.

It can be seen that for most cases it is obvious to consider optimal DOPID instead of optimal FPID controller as one obtains either less fluctuating, either faster response. For optimization problem 4 that includes more constraints it is only possible to find optimal DOPID controller.

## VI. CONCLUSION

This paper shows the comparison of optimal DOPID and FPID controllers for different optimization problems. It is shown that there are benefits of using DOPID controller for most cases with regular number of constraints. For the case for larger number of constraints it is only possible to find optimal DOPID controller.

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## REFERENCES

- [1] Aström K. J., T. Hägglund, *PID controllers: theory, design and tuning*, Instrument Society of America, North Carolina (1995)
- [2] Aström K. J., T. Hägglund, *Advanced PID Control*, Instrument Society of America, North Carolina, ISA (2005)

- [3] B. B. Jakovljević, M. R. Rapačić, Z. D. Jeličić, T. B. Šekara, "Optimization of distributed order fractional PID controller under constraints on robustness and sensitivity to measurement noise", *Fractional Differentiation and Its Applications (ICFDA), 2014 International Conference on*, (Catania, Italy, 2014. )
- [4] B. B. Jakovljević, M. R. Rapačić, Z. D. Jeličić, T. B. Šekara, "Optimization of fractional PID controller by maximization of the criterion that combines the integral gain and closed-loop system bandwidth", *System Theory, Control and Computing (ICSTCC), 2014 18th International Conference* , (18, Sinaia, Romania, 2014 ).
- [5] B. B. Jakovljević, T. B. Šekara, Z. D. Jeličić, M. Č. Bošković, M. N. Kapetina, "Distributed order PID optimization by minimization of combination of integral of positive and negative response parts", *International Conference on Fractional Differentiation and its Applications (ICFDA2016)*, (Novi Sad, Serbia, July 18 - 20, 2016).
- [6] B. B. Jakovljević, M. R. Rapačić, M. N. Kapetina, T. B. Šekara, "Usporedna analiza performansi jedne klase linearnih optimalnih regulatora celog i necelog reda", *INFOTEH-JAHORINA*, **13**(SUP-3), 2014.
- [7] B. B. Jakovljević, "Optimal and suboptimal parameter tuning of robust, linear controllers of noninteger order", *PhD thesis* University of Novi Sad, Faculty of Technical Sciences, Serbia, 2015.
- [8] Šekara T. B. and M. R. Mataušek, "Revisiting the Ziegler-Nichols process dynamics characterization", *Journal of Process Control* **20**, pp. 360-363, 2010

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